

# Adsorption and Desorption Studies of Heavy Metals on to Coconut Shell Char

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## ABSTRACT

Heavy metals in wastewater can be removed by several methods including adsorption. Activated carbon (AC) is widely used, but expensive adsorbent. Since AC derived from coconut shell (CS) is a good adsorbent, coconut shell char (CSC) as well might be an effective low-cost adsorbent. It was studied the possibilities of using CSC as an adsorbent. Results showed that, CSC has 13% and 12% removal efficiencies for Zn<sup>2+</sup> and Ni<sup>2+</sup> from solutions of 50 mg/l. Furthermore, desorption abilities of H<sub>2</sub>SO<sub>4</sub>, NaOH, Distilled water and NaCl as desorbing agents were analysed and found H<sub>2</sub>SO<sub>4</sub> to be the most effective desorbing agent.

**Key words:** Adsorption, Desorption, Coconut shell char

## INTRODUCTION

Heavy metals are one of the most hazardous contaminants released to water bodies by anthropogenic activities. (Burakov et al., 2018). Therefore, various methods have been used to remove heavy metals from aqueous media. However, due to the advantages like low cost, easy operation conditions, wide pH range, high metal binding capacity and reusability of adsorbents, adsorption has become a more preferred treatment method (Barakat, 2011) (Carolin et al., 2017). AC is found to be an efficient adsorbent to remove heavy metal ions due to its porous structure and high specific area. However, utilizing AC is limited in developing countries due to its high preparation cost (Srivastava et al., 2008). Therefore, considering that, AC derived from CSC has good adsorption properties; the study was carried out to check the adsorption ability of CSC. As well as the adsorption ability, desorption properties of CSC were tested with different desorbing agents: H<sub>2</sub>SO<sub>4</sub>, NaOH, NaCl and distilled water. The main objective of the study is to evaluate the heavy metal adsorption and desorption properties of CSC while, identifying a suitable desorption agent. Among the most common heavy metals present in the wastewater Ni<sup>2+</sup> and Zn<sup>2+</sup>

are used for the studies.

## METHODOLOGY

### Material preparation

#### *Preparation of the adsorbent*

Required CSC was obtained from a supplier in Gampaha. Washed and dried char was grinded to particles in the range of 500 - 1000 μm. Then, char was washed with tap water followed by distilled water before oven drying at 50 – 60 °C until a constant weight was obtained.

#### *Preparation of solutions*

200 mg/l Zn<sup>2+</sup> and Ni<sup>2+</sup> solutions were prepared by dissolving 1.820 g of analytical grade Zn(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O and 1.982 g of analytical grade Ni(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O obtained from Sigma Aldrich Corporation in 2 l of distilled water separately. 0.1 M H<sub>2</sub>SO<sub>4</sub>, 0.1 M NaOH, 0.5 M NaCl and distilled water were selected as desorption agents. 1 l solutions of each agent were prepared using analytical grade solutions or chemicals.

### Adsorption studies

#### *Effect of Initial solute concentration*

200 ml of 25, 50 and 100 mg/l  $Zn^{2+}$  and  $Ni^{2+}$  solutions were prepared using 200 mg/l stock solution. Inherent pH of each solution was measured. Each sample was mixed with 2 g of adsorbents at 150 rpm stirrer speed for 2 hours. Finally, sample solutions were filtered using a filter paper and each filtrate was analyzed.

#### *Effect of Contact Time*

2 l of 50 mg/l  $Zn^{2+}$  and  $Ni^{2+}$  solutions with an initial pH of 5 were prepared. Each sample was loaded with 19 g and mixed at 150 rpm stirrer speed. 50 ml of samples were withdrawn at time 0, 1, 2, 3, 5, 10 and 20 minutes for the study.

#### **Desorption studies**

Used adsorbents were prepared by contacting 1.9 l of 50 mg/l  $Zn^{2+}$  and  $Ni^{2+}$  solutions with 19 g of adsorbents separately. pH, stirrer speed and contacting time was maintained as 5, 150 rpm and 4 hours. After the operation adsorbents were separated by filtration and oven dried at 80 - 100 °C until, the weight becomes constant. 0.1 M  $H_2SO_4$ , 0.1 M NaOH, 0.5 M NaCl and distilled water were used as desorption agents. For 4 g of adsorbent, 100 ml of desorption agent with stirring speed of 150 rpm and 4 hours contacting time.

## **RESULTS AND DISCUSSION**

### **Adsorption studies**

#### *Effect of initial metal ion concentration*

According to Figure 1, Ion removal percentage decreases when the initial ion concentration increases for both solutes. The ratio of surface-active sites to the total metal ions in the solution is high in low ion concentrations. Therefore, all metal ions may interact with the adsorbent and be removed from the solution. Moreover, in low concentrations removal of  $Zn^{2+}$  is more effective than  $Ni^{2+}$ . Furthermore, as shown in the Figure 2 amount of metal

adsorbed per unit weight of adsorbents (adsorption capacity) decreases with increasing initial metal ion concentration. However, for  $Ni^{2+}$ , there is no sharp variation as in  $Zn^{2+}$  in adsorption capacity.  $Ni^{2+}$  adsorption capacity is around 0.5 mg  $Ni^{2+}$ / g CSC for any initial metal ion concentration. The reason may be higher electro negativity of  $Ni^{2+}$  than  $Zn^{2+}$ . Therefore, it readily attached with available anionic

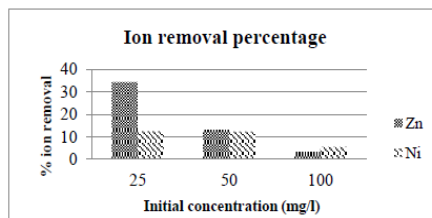


Figure 1 Variation of percentage ion removal with initial ion concentration

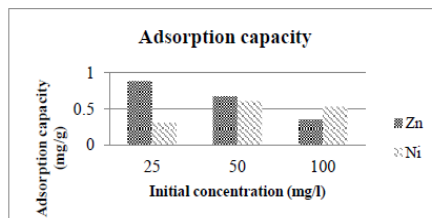


Figure 2 Variation of adsorption capacity with initial ion concentration

functional groups (-OH) on the surface of CSC.

#### *Effect of contact time*

Initial concentration of the  $Zn^{2+}$  and  $Ni^{2+}$  solutions were 47 and 54 mg/l respectively. With time a rapid adsorption can be seen in  $Zn^{2+}$  ions in first 5 minutes as shown in Figure 3. However, a sudden desorption, resulted increase of ion concentration within next 15 minutes.  $Ni^{2+}$  adsorption kinetics shows a rapid adsorption initially in first three minutes and then desorption become dominant in next few minutes. For final 15 minutes, solution concentration is around equilibrium concentration of corresponding initial ion

### Desorption Studies.

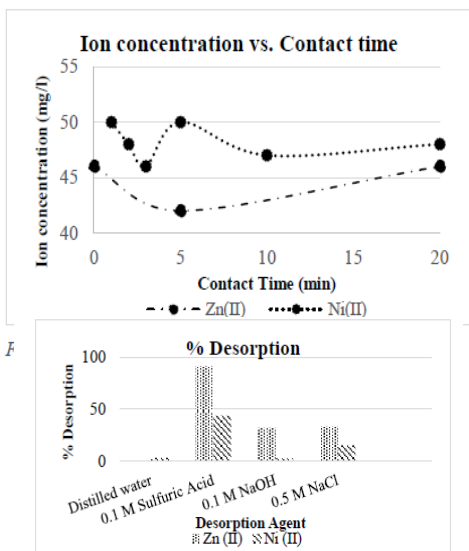


Figure 4 % Desorption for different desorption agent

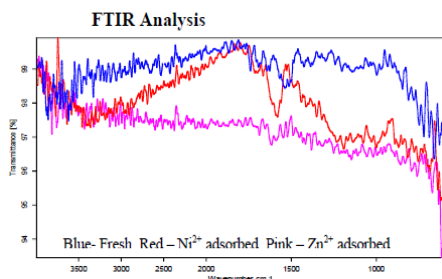


Figure 5 Results of FTIR analysis

As shown in Figure 4, Sulfuric acid is the best desorption agent with 90% and 44% desorption of adsorbed Zn<sup>2+</sup> and Ni<sup>2+</sup> respectively. It may be due to attraction and strong bond between H<sup>+</sup> and OH<sup>-</sup> ions. Being neutral, distilled water is the poorest desorption agent. According to results it can be identified that more ionic and acidic the agent, desorption ability is higher.

Bands between 3500 – 3000 cm<sup>-1</sup> are related to the valence vibrations of the –OH groups. After adsorption, the displacement of vibration bands can be

observed for both Zn<sup>2+</sup> and Ni<sup>2+</sup>. It may be due to the formation of chemical bonds between functional groups present in CSC.

### CONCLUSIONS

According to the results it can be suggest that high dose CSC is required for effective removal of heavy metals. Because, in commercial scale, percentage ion removal should be at least higher than 80%. Desorption studies emphasis that acids are the most suitable desorption agent. However, AC derived from CS is one of the best commercial AC. Hence study can extend further to examine adsorption characteristic of CSC treated by various chemicals and temperatures.

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